

PHASE BEHAVIOR IN PETROLEUM FLUIDS: A DETAILED DESCRIPTIVE AND ILLUSTRATIVE ACCOUNT WITH EMPHASIS ON HEAVY ORGANICS

G. Ali Mansoori

Departments of BioEngineering, Chemical Engineering & Physics, University of Illinois at Chicago, Chicago, IL 60607-7052 USA

Keywords: Aggregation; Alkane; Aromatic hydrocarbon; Asphaltene; Cloud point; Gas-condensate, Deposition; Diamondoid; Dynamic pour point; First order phase transition; Flocculation, Gas-condensate; Heavy oil; Heavy organic; Hydrocarbon; Infinite-order phase transition; Intermediate crude; Light crude; Natural gas; NGL, Oil; Oil shale; Onset of deposition; Paraffin; Petroleum fluid; Phase behavior; Phase-transition; Phase transition points, Polydisperse fluid; Polymer solution; Precipitation; Resin; Second order phase transition; Solid formation; Static pour point; Tar sand; Thermodynamics; Wax.

Contents

- 1. Introduction
- 1.1. Naturally Occurring Petroleum Fluids
- 2. Components of Petroleum Fluids
- 2.2. Impurities in Petroleum Fluids
- 2.3. Heavy Fractions in Petroleum Fluids
 - 2.3.1. Petroleum Wax
 - 2.3.2. Diamondoids
 - 2.3.3. Asphaltenes
 - 2.3.4. Petroleum Resins
- 3. Phase Behaviors in Petroleum Fluids
 - 3.1. Temperature Effect on Petroleum Fluids Phase Separation:
 - 3.2. Pressure Effect on Petroleum Fluids Phase Separation:
 - 3.3. Theory of Phase-Transitions
 - 3.4. Phase-Transition Points
- 4. Discussion
- Glossary
- Bibliography
- Biographical Sketch

Summary

This chapter presents a descriptive and illustrative account of phase behavior in the seven naturally occurring petroleum fluids and ties all the known eleven phase-transition concepts in a unified narrative. The figures and tables contained in this report are designed so that they could effectively support the discussion about molecular make-up of petroleum fluids, P- and T-effects on phase behavior and phase transition points.

Seven naturally occurring hydrocarbon fluids are known as petroleum fluids. They

include, in the order of their fluidity, natural gas, gas-condensate (NGL), light crude, intermediate crude, heavy oil, tar sand and oil shale. In this report we present a generalized description of the various phase transitions, which may occur in petroleum fluids with emphasis on heavy organics deposition.

At first the nature of every petroleum fluid is presented. Their constituents including their so-called impurities are identified and categorized. Heavy fractions in petroleum fluids are discussed and their main families of constituents are presented including petroleum wax, diamondoids, asphaltenes and petroleum resins.

Then the generalized petroleum fluids phase behavior is discussed in light of the known theory of phase transitions. The effects of variations of composition, temperature and pressure on the phase behavior of petroleum fluids are introduced.

Finally eleven distinct phase-transition points of petroleum fluids are presented and their relation with state variables and constituents of petroleum fluids are identified. This report is to generalize and relate phase behaviors of all the seven naturally occurring petroleum fluids into a unified perspective. This work is the basis to develop a comprehensive computational model for phase behavior prediction of all the petroleum fluids, which is of major interest in the petroleum industry.

1. Introduction

The petroleum and natural gas literature is quite rich in data, industrial correlations and molecular-based prediction methods of the liquid-vapor phase behavior of petroleum fluids (see [1]-[17]). For this reason little effort is made to discuss further liquid-vapor equilibrium in this report. Our emphasis is to introduce a generalized perspective about all the variety of phase transitions, which may occur in the seven category of naturally occurring petroleum fluids. This includes vapor separation, solid crystalline deposition, colloidal and micellar solutions formation as well as aggregation, flocculation and non-crystalline solid formation and separation.

We are in the process of developing a comprehensive phase behavior prediction package for petroleum fluids, which can be applied to any of the seven categories of such fluids from underground natural reservoirs. Having a thorough understanding of all the possible phase transitions in the seven categories of petroleum fluids will allow us to formulate the necessary computational package for their phase behavior prediction regardless of the kind, source, nature of components and thermodynamic conditions.

1.1. Naturally Occurring Petroleum Fluids

There exist seven well-known petroleum fluids in nature. In the order of their fluidity, they are natural gas, gas-condensate (also known as NGL standing for natural-gas liquid), light crude, intermediate crude, heavy oil, tar sand and oil shale as shown symbolically in Figure 1. These are all naturally occurring complex mixtures made up of hydrocarbons and other organic and inorganic compounds with variety of molecular structures and sizes.



Figure 1. The normal conditions of the seven naturally occurring petroleum fluids, in the order of fluidity from left to right, natural gas, gas-condensate (NGL), light crude oil, intermediate crude oil, heavy oil, tar sand and oil shale.

The hydrocarbons and most other organic compounds present in all these seven naturally occurring petroleum fluids are generally polydispersed having a range of size, shape and molecular weight distributions (see for example [18]). As a result continuous functions may be used for their mole fraction distributions (see for example [19-24]). In Figure 2 we report the approximate relative composition of various petroleum fluids with respect to the number of carbon atoms of their organic contents.

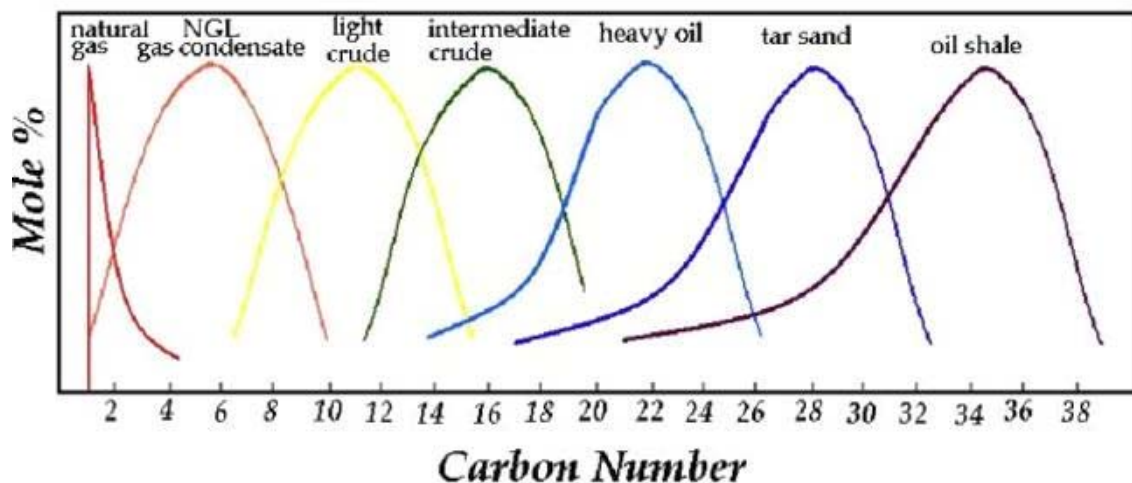


Figure 2. Various categories of natural gas and liquid hydrocarbon reserves and their approximate hydrocarbon molecular weight distributions according to their carbon numbers

We think this is a useful way to classify petroleum fluids according to their composition. This novel classification will allow us to look at all the petroleum fluids from a unified basis which is their hydrocarbon contents and their relative distribution. According to this figure, the molecular weight of hydrocarbons present in petroleum fluids increases from left to right in the list of the seven. It should be also mentioned that heavy oil, tar sand and oil shale contain appreciable amounts of resins and asphaltenes, while the percentages of these compounds are generally low in the lighter petroleum fluids.

Petroleum fluids vary in color, odor, and physicochemical properties. Generally many compounds are known to be present in petroleum fluids. The number of carbon atoms in the hydrocarbons and other organic compounds present in petroleum fluids can vary

from one (as in methane) to over a hundred (as in asphaltenes and heavy paraffins) [25, 26].

During their production, transportation and processing petroleum fluids may go through a number of phase changes, which include evaporation (separation of gases from liquid streams), retrograde condensation (separation of liquids from gas streams) and solids formation and deposition (separation of crystalline solids, colloids and aggregates from liquid or vapor streams). The latter is mostly due to precipitation and / or deposition of diamondoids, wax and asphaltenes. In view of the complexity of petroleum fluids, study and understanding of their phase behavior is still a challenging and an industrially important task. Such an understanding will help us to design a more economical route for the related production, transportation and refining projects. The complexity of the phase behavior in petroleum fluids is due to the existence of the variety and polydispersity of hydrocarbons and other organic molecules in them. In this report, we present the various phase-transitions, which may occur in petroleum fluids, and we introduce a unified perspective of their phase behaviors. This may allow us to develop a comprehensive theoretical model for phase behavior prediction of all the petroleum fluids which is of major concern in the petroleum industry.

2. Components of Petroleum Fluids

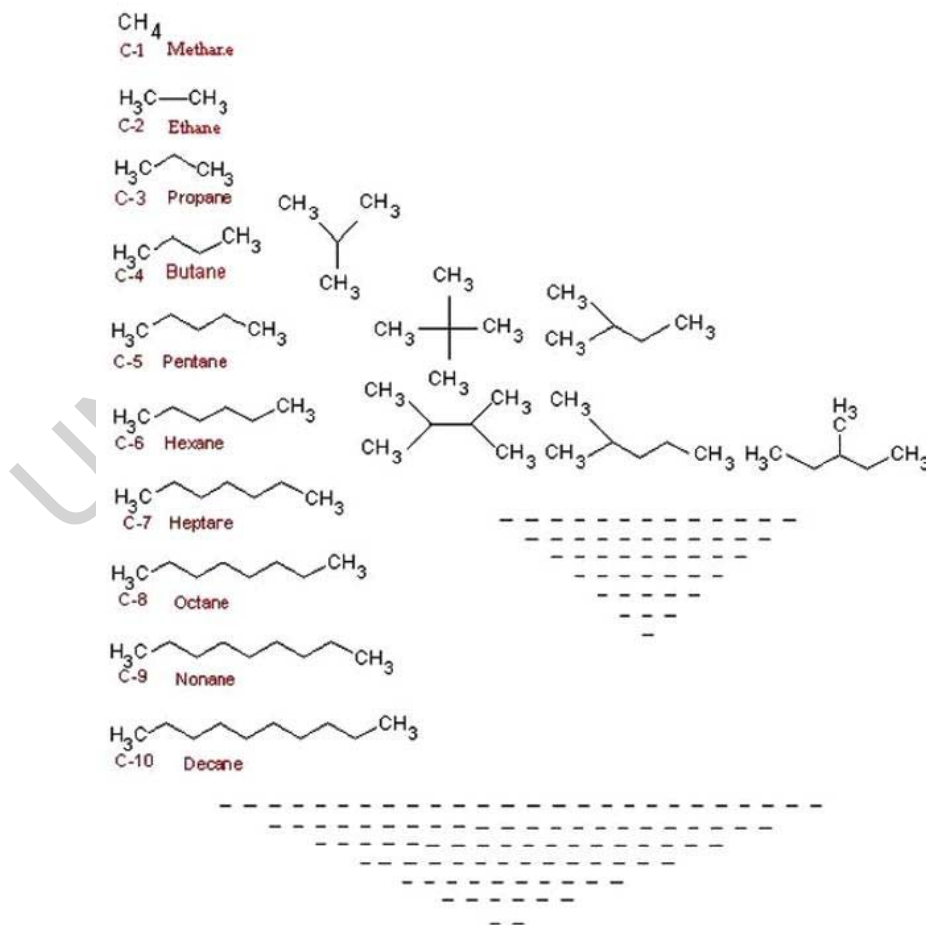


Figure 3. Lighter paraffin hydrocarbons present in petroleum fluids

The predominant hydrocarbons present in lighter petroleum fluids (natural gas, gas-condensate, light-crude and intermediate-crude oil systems) are alkanes (also known as paraffin hydrocarbons) as shown in Figure 3.

As we look at the physical properties of petroleum fluids, going from natural gas to oil shale, their alkanes content decrease while their viscosity and density increase. Other hydrocarbons present in petroleum fluids are aromatic hydrocarbons (see Figure 4) at somehow lower concentrations than paraffins depending on the underground natural reservoir source. Other families of hydrocarbons are also present in petroleum fluids but their concentrations are generally rather low.

Quite frequently, petroleum fluids contain various amounts of other organic and inorganic compounds, which are usually termed as impurities from the petroleum industry point of view.

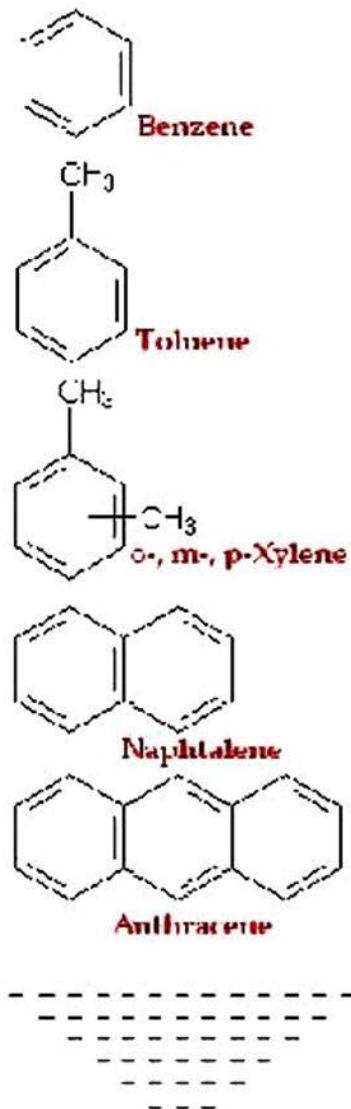


Figure 4. Lighter aromatic hydrocarbons present in petroleum fluids

2.2. Impurities in Petroleum Fluids

All the non-hydrocarbon organic and inorganic components of petroleum fluids are considered impurities from the petroleum industry perspective. Molecular structure of organic impurities is composed of mostly such elements as carbon, hydrogen, metals, nitrogen, oxygen and sulfur. Molecules of inorganic impurities are generally composed of carbon, metals, oxygen and sulfur. Petroleum fluid impurities can be categorized into five groups of compounds:

- (i) The major low molecular weight impurities, which include carbon dioxide (CO₂), hydrogen sulfide (H₂S), metal oxides (Al₂O₃, Fe₂O₃, SiO₂, etc.), nitrogen (N₂), oxygen (O₂), salts (NaCl, CaCO₃, etc.), sulfur (S) and water (H₂O).
- (ii) High molecular weight impurities, which could be present in the petroleum fluids heavy fractions. They include asphaltenes, asphaltogenic acids, diamondoids and derivatives, mercaptans, metal carbenes, organometallics, petroleum resins and wax. In Table I the general closed chemical formulae of high molecular weight impurities of petroleum fluids are presented.
- (iii) There may be also other organic and inorganic compounds present in petroleum fluids, which depend on their underground natural reservoir source. The concentration of such other organic matter is generally rather low and they have little or no effect on petroleum fluids phase behavior.
- (iv) Another category of impurities which may be present are compounds which have been added to petroleum fluids during their production, transportations and storage stages for various reasons. These include but not limited to acids, alcohols, aromatic hydrocarbons, detergents and polymers.
- (v) Petroleum fluids often contain compounds, which are a result of physical association of hydrocarbons and the above-mentioned impurities and contaminants. They include clatherates, colloids, crystalline solids, flocs and slugs.

High Mw Impurity	General Closed Formula
Asphaltenes	$C_m H_n N_i O_j S_k$
Asphaltogenic Acids	$C_m H_n N_i O_j S_k - COOH$
Diamondoids	$C_{4n+6} H_{4n+12}$
Mercaptans	$C_m H_n N_i O_j S_k X$
Metal Carbenes	$R_1 HC=CHR_2 X$
Organometallics	<i>Ex.:</i> $R_1 - X - R_2$
Petroleum Resins	$C_m H_n N_i O_j S_k$ $i, j, k = 0$ or 1
Wax	$C_m H_n$ $18 \leq m \leq 60$ $n \leq 2m + 2$

Table 1: General closed chemical formulae of high molecular weight impurities of petroleum fluids. In this table C is carbon, H is hydrogen, N is nitrogen, O is oxygen, S is sulfur and X is metals and R represents a hydrocarbon segment.

As it was mentioned above the literature on petroleum and natural gas is rich of

numerous data banks, correlations, and nomograms for the analysis and treatment of petroleum fluids and their liquid-vapor phase behavior.

The presentation given in this report is an attempt to relate properties and phase behavior of petroleum fluid systems to the molecular behavior of the compounds present in them. This would allow us to make a unified and a science-based generalization of the behavior of petroleum fluids.

One of the important fractions of petroleum fluids, which is the least understood is their heavy fraction. Because of the complexity of the heavy fractions, we discuss them in more detail in the following separate section.

2.3. Heavy Fractions in Petroleum Fluids

To perform an accurate prediction of the phase behavior of petroleum fluids we need to know the nature and composition of the molecules, which make up the petroleum heavy fractions [27]. There is a wealth of information and database available for the light and intermediate components of petroleum fluids [1-17].

The investigation of the accurate chemical constitution of petroleum heavy fractions is hindered by their complex nature. Almost all the molecules comprising the heavy fractions of petroleum fluids are polydispersed [18, 27, 28, 29].

The predominant part of the high molecular weight impurities (known as heavy fractions or petroleum residuum) are asphaltenes, asphaltogenic acids/compounds, diamondoids and derivative, heavy aromatic hydrocarbons, mercaptans, metal carbenes / organometallic, petroleum resins and wax. In Table 1 we report the general closed chemical formulae of these compounds.

It is generally understood that heavy fractions have little or no effect on the liquid-vapor phase behavior of the majority of petroleum fluids. Their main contribution is in the solids separation from petroleum fluids, due to changes in the composition, temperature and pressure.

The main components of the heavy fraction, which participate in the solid phase formation, include asphaltenes, diamondoids, petroleum resins and wax. In what follows we present a more detailed description of their molecular characteristics and their physical properties.

2.3.1. Petroleum Wax

Petroleum wax is a class of mineral wax that is naturally occurring in the heavy fractions of petroleum fluids [30-37]. They vary compositionally over a wide range of molecular weights up to hydrocarbon chain lengths of approximately C₆₀ [34]. Petroleum wax is made up mostly of saturated paraffin hydrocarbons with their number of carbon atoms in between 18-36 (see Figure 5).

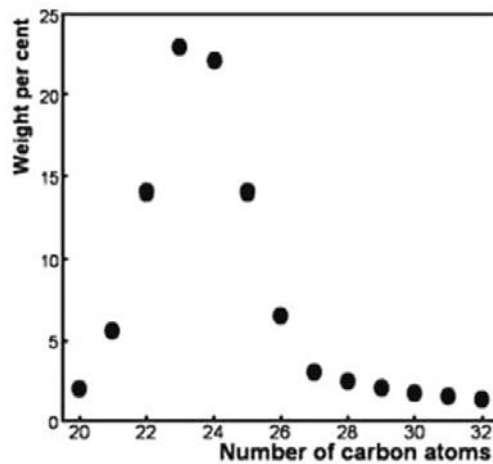


Figure 5. The distribution of n-alkanes in Suntech P116 paraffin wax as a function of the number of carbon-atoms (Taken from [32])

Wax may also contain small amounts of naphthenic hydrocarbons with their number of carbon atoms in the range of 30-60. Wax usually exists in intermediate crudes, heavy oils, tar sands and oil shales. Petroleum wax is typically in solid state at room temperature and it is separated from relatively high boiling petroleum fractions during the refining processes. Petroleum wax, like most other components of heavy end of petroleum fluids, is polydispersed. As an example, we report in Figure 5 the distribution of n-alkanes as a function of the number of carbon-atom compounds in a paraffin wax sample.

-
-
-

TO ACCESS ALL THE 29 PAGES OF THIS CHAPTER,
Visit: <http://www.eolss.net/Eolss-sampleAllChapter.aspx>

Bibliography

- [1]. R.R. Agahi, B. Ershaghi, M.C. Lin and A. Mansoori, (1995) "Thermodynamic behavior of hydrogen / natural gas mixtures, Proceedings of the 74th Annual Convention of the Gas Processors Association, GPA, Tulsa, OK, pp. 23-27 . [Equation of state approach to predict the behavior of hydrogen mixed with natural gas].
- [2]. American Petroleum Institute Publications: see www.api.org/Publications/ [API publications are rich in information about liquid-vapor phase behavior of petroleum fluids].
- [3]. Benmekki, E.H., Mansoori, G.A., (1986). SPE Paper # 15677. Accurate Vaporizing Gas-Drive Minimum Miscibility Pressure Prediction. Society of Petroleum Engineers, Richardson, TX. [Application of statistical mechanical mixing rules and three-body forces for minimum miscibility pressure prediction of hydrocarbon mixtures].
- [4]. A. Danesh, (1998) PVT and Phase Behaviour of Petroleum Reservoir Fluids, *Elsevier Science* (May 1, 1998). [This discusses vle phase behavior, pvt tests and correlations, fluid characterization, gas

injection, and reservoir simulation applications.].

[5]. M. Edalat, R.B. Bozar-Jomehri and G.A. Mansoori, (1993) "Generalized equation predicts vapor pressure of hydrocarbons and other liquids" *Oil & Gas Journal*, Feb. 1, pp.39-40. [This presents the most general vapor pressure correlation for all possible liquids].

[6]. R. Hartono, G.A. Mansoori and A. Suwono, (1999) "Prediction of Molar Volumes, Vapor Pressures and Supercritical Solubilities of Alkanes by Equations of State" *Chemical Engineering Communications*, Vol. 173, pp. 23-42. [This demonstrates the high accuracy of equations of state presented in [11] and [15] for petroleum fluids density, vle, retrograde condensation and supercritical fluid solubility calculations].

[7]. Hoffman, A.E., Crump, J.S., Hocott, C.R., (1953). Equilibrium Constants for a Gas-Condensate System. *Trans. AIME*, 198: 1-10. [An excellent set of experimental data for gas condensate and its phase behavior].

[8]. H. Manafi, G.A. Mansoori and S. Ghotbi, (1999) Phase behavior prediction of petroleum fluids with minimum characterization data. *J. Pet. Sci. Eng.* **22** ,pp. 67–93. [The most accurate prediction technique for all petroleum fluids vle phase behaviors].

[9]. Magoulas, K., Tassios, D., (1990). Thermophysical Properties of n-alkanes from C₁-C₂₀ and their prediction to higher ones. *Fluid Phase Equilibria*, 56: 119-140 [An excellent collection of data and correlations].

[10]. W. D. McCain, (1990) *The Properties of Petroleum Fluids*, Pennwell Books, (April 1990). [Contents include water-in-crude-oil emulsions, characterization, phase behavior, and field processing of crude oil, separation of gas, oil and water, dehydration and desalting of crude oil, crude sweetening and stabilization, pumps, measurement of crude oil, fire heaters, pipeline transportation, energy conservation, instrumentation and process control, pressure relief and flaring, case histories].

[11]. M. Mohsen-Nia, H. Modarress and G.A. Mansoori, (1993) "A simple cubic equation of state for hydrocarbons and other compounds", SPE paper No. 26667, Proceedings of the 1993 Annual SPE Meeting, Society of Petroleum Engineers, Richardson, TX. [The most accurate two-parameter cubic equation of state for all fluids and mixtures].

[12]. M. Mohsen-Nia, H. Modarress and G.A. Mansoori, (1994) "Sour, hydrogen containing and liquified natural gas equation of state", *J. Petrol. Science & Engineering*, Vol. 12, pp. 127-136. [An accurate equation of state for sour natural gas and liquid].

[13]. K.S. Pedersen and P.L. Christensen, (2006) *Phase Behavior of Petroleum Reservoir Fluids*, CRC Press, (November 1, 2006). [This discusses sampling, characterization, compositional analyses, and equations of state used to simulate various pvt properties of reservoir fluids].

[14]. A.P. Pires, R.S. Mohamed and G.A. Mansoori, (2001) "An equation of state for property prediction of alcohol/hydrocarbon and water/hydrocarbon systems" *J. Petrol. Sci. & Eng.*, Vol.32, pp.103-114. [An accurate equation of state developed for high and low pressures phase behavior predictions of alcohol/hydrocarbon and water/hydrocarbon mixtures].

[15]. Riazi, M.R. and Mansoori, G.A., (1993). Simple equation of state accurately predicts hydrocarbon densities" *Oil & Gas Journal*, 108-111, July 12. [The most accurate equation of state for density prediction of hydrocarbons and their mixtures].

[16]. Roland, C.H., (1942). Vapor-Liquid Equilibria for Natural Gas -Crude Oil Mixtures. *Ind. Eng. Chem.* 37, 10: 930-936. [A set of excellent experimental data for the said petroleum fluids].

[17]. Twu, C.H., (1984). An Internally Consistent Correlation for Predicting the Critical Properties and Molecular Weights of Petroleum and Coal-Tar Liquids. *Fluid Phase Equilibria*, 16: 137-150. [The title is self-explanatory]

[18]. G. A. Mansoori, D. Vazquez and M. Shariaty-Niassar, (2007) "Polydispersity of heavy organics in crude oils and their role in oil well fouling", *J. Petrol. Sci. and Engg*, Volume 58, Issues 3-4, September 2007, Pages 375-390. [A unique and detailed methodology and data to understand and quantify the role of polydispersity of heavy organics in their deposition from petroleum fluids].

[19]. Du, P.C., Mansoori, G.A., (1986). Phase Equilibrium Computational Algorithms of Continuous Mixtures. *Fluid Phase Equilibria*, 30: 57-64. [Development of three fundamental theories of

reformulating the Gibbs phase equilibrium conditions for polydisperse mixtures and their applications for petroleum fluids].

[20]. Du, P.C., Mansoori, G.A., (1987). Phase Equilibrium of Multicomponent Mixtures: Continuous Mixture Gibbs Free Energy Minimization and Phase Rule. *Chem. Eng. Comm.* 54. pp: 139-148; .

Mansoori, G.A., Du, P.C. and Antoniadis, E., (1989). Equilibrium in Multiphase Polydisperse Fluids. *International Journal of Thermophysics*, 10: No. 6, 1181-1204. [Principle of reformulating the Gibbs free energy minimization criteria for continuous mixtures and its applications for petroleum fluids].

[21]. Heynes, Jr., H.W., Matthews, M.A., (1991). Continuous Mixture Vapor-Liquid Equilibria Computations Based on True Boiling Point Distillations. *Ind. Eng. Chem. Res.*, 30: 1911-1915.

[22]. Peng, D.Y., Wu, R.S., Batcky, J.P., (1987). Application of Continuous Thermodynamics to Oil Reservoir Fluid Systems using an Equation of State. *AOSTRA J. Res.*, 3: 113-122.

[23]. G.R. Vakili-Nezhaad, H. Modarress, G.A. Mansoori, (2001) Continuous thermodynamics of petroleum fluids fractions, *Chemical Engineering and Processing*, 40, 431-435. [A novel technique for application of continuous mixture theory for petroleum fractions].

[24]. William, B.T., Teja, S.A., (1986). Continuous Thermodynamics of Phase Equilibria Using a Multivariate Distribution Function and an Equation of State. *AIChE J.*, 32: 2067-2078.

[25]. N. Berkowitz, (1997) *Fossil Hydrocarbons*, Academic Press; 1st edition (January 15, 1997). [Contents include the family of fossil hydrocarbons, the chemical precursors, the biosources, diagenesis, biomarkers, catagenesis, the "heavy: hydrocarbons, about formation of oil].

[26]. A. Firoozabadi, (1999) *Thermodynamics of Hydrocarbon Reservoirs*, McGraw-Hill. [Contents include equilibrium, nonequilibrium, and irreversible processes].

[27]. Chorn, L.G., Mansoori, G.A. (1989). Multicomponent Fractions Characterization: Principles and Theories. C7+ Fraction Characterization. *Advances In Thermodynamics* Vol:1. Taylor & Francis Press, New York, N.Y. pp: 1-10

[28]. D. Vazquez, J. Escobedo and G.A. Mansoori, (1998) Characterization of crude oils from southern Mexican oilfields. In: *Proceedings of the EXITEP 98, International Petroleum Technology Exhibition, Placio de Los Deportes, Mexico City, Mexico, D.F., 15th–18th November*, PEMEX, Mexico City.

[29]. D. Vasquez and G.A. Mansoori, (2000) Identification and measurement of petroleum precipitates. *J. Pet. Sci. Eng.* 26 1–4 , pp. 49–56. [This gives a thorough methodology and experimental procedure for quantitative identification and measurement of petroleum precipitates].

[30]. J. R. Becker, (1997) *Crude Oil Waxes, Emulsions, and Asphaltenes*, Pennwell Books [Contents include petroleum companies and emulsions forces involved in macroscopic physical behavior of emulsions, oil and water emulsion breakers, petroleum companies and waxes, chemical surfaces, wax crystal order and temperature, wax physical properties and quantum effects, asphaltenes and crude oil, asphaltenes bulk behavior and testing methods, physical properties of treating chemicals].

[31]. B.J. Fuhr, L. Cathrea, K.H. Coates and A.I. Majeed, (1991) Properties of asphaltenes from a waxy crude. *Fuel* 70, pp. 1293–1301.

[32]. S. Himran, A. Suwono, and G.A. Mansoori, (1994) "Characterization of alkanes and paraffin waxes for application as phase change energy storage medium", *Energy Sources*, Vol. 16, pp. 117-128. [The title is self-explanatory]

[33]. G.A. Mansoori, (1996) "Asphaltene, resin, and wax deposition from petroleum fluids" *The Arabian Journal for Science and Engineering*, Vol. 21, Number 48, pp. 707-723, December 1996. [A detailed description of mechanisms, theories and models for asphaltene, resin and wax deposition].

[34]. G. A. Mansoori, H. Lindsey Barnes and Glen M. Webster, (2003) "Petroleum Waxes" Chapter 19 in *"Fuels and Lubricants Handbook"*, ASTM Int'l, West Conshohocken, PA, Pages 525-558. [A detailed review of the state of the art on properties, characterization, separations and measurements of petroleum waxes].

[35]. R.J. Cole and F.W. Jessen, (1960) Paraffin deposition. *Oil Gas J.* 58 , pp. 87–99. [An early study of paraffin deposition and methods to combat it].

- [36]. E.B. Hunt, Jr., (1962) Laboratory study of paraffin deposition. *J. Pet. Technol.* **225** , pp. 1259–1267.
- [37]. D.A. Shock, J.D. Sadbury and J.S. Crockett, (1955) Studies of the mechanism of paraffin deposition and its control. *J. Pet. Technol.* **7** 9 , pp. 23–30. [a state-of-the-art review of the subject].
- [38]. G. A. Mansoori, (2007) “Diamondoid Molecules” in *Advances in Chemical Physics*, 136, pp. 207-258. [A detailed review and collection of data on properties, separations, mechanisms, models and prospects for diamondoids molecules].
- [39]. G.A. Mansoori, T.F. George, G. Zhang and L. Assoufid, (2007) *Molecular Building Blocks for Nanotechnology: From Diamondoids to Nanoscale Materials and Applications* (Springer, New York), Topics in Applied Physics 109. [A collection of research papers on the subject matter of the book].
- [40]. G.R. Vakili-Nezhaad, B. Soltani, G.A. Mansoori and K. Kiani-Nasab, (2005) Investigation on the Existence of Diamondoids in Crude Oils, *Int'l J. Nanoscience and Nanotechnology*, 1(1):65-74.
- [41]. W. Bungler, (1982) *Chemistry of Asphaltenes* (Advances in Chemistry Series), American Chemical Society. [This is a collection of research papers].
- [42]. K.J. Leontaritis and G.A. Mansoori, (1987) Asphaltene flocculation during oil recovery and processing: a thermodynamic-colloidal model SPE Paper #16258 . In: *Proceedings of the SPE Symposium on Oil Field Chemistry*, Society of Petroleum Engineers, Richardson, TX.
- [43]. G.A. Mansoori, (1994) "The occurrence of asphaltene throughout production cycle", Proceedings of the 6th ADIPEC, pp. 282-292, Society of Petroleum Engineers, Richardson, TX. [A state-of-the-art review of mechanisms, theories and models for the role of asphaltene in petroleum production].
- [44]. O.C. Mullins and E.Y. Sheu, (1999) *Structures and Dynamics of Asphaltenes*, Springer; 1 edition (January 31, 1999).
- [45]. O.C. Mullins, E.Y. Sheu, A. Hammami and A.G. Marshall, (2006) *Asphaltenes, Heavy Oils, and Petroleomics*, Springer. [A collection of technical papers].
- [46]. M.K. Sharma and T.F. Yen, (1994) *Asphaltene Particles in Fossil Fuel Exploration, Recovery, Refining, and Production Processes (The Language of Science)*, Springer.
- W. H. Bragg and W. L. Bragg, (1913) *The Structure of the Diamond Nature*, 91, 557-557. [The first attempt for the use of X-rays to the case of the diamond in order to establish its structure.].
- [47]. Yen, T.F., and Chilingarian, G.V.(editor), (1994) "*Asphaltenes and Asphalt*, 1", Elsevier Science, Amsterdam, pp. 95-110. [A state-of-the-art collection of research papers].
- [48]. T. Suzuki, Y. Ito, Y. Takegami and Y. Watanabe, Chemical structure of tar–sand bitumens by ¹³C and ¹H NMR spectroscopy method. *Fuel* **61** (1982), pp. 402–410.
- [49]. J.J. Altamirano, M.A. Flores, O. Pie, N. Panivino, C. Arzate, G. Kapellman, M.T. Lopez, S. Spinoza and S. Rosales, (1986) *Revisita del Instituto Mexicano del Petroleo*, 18, 2 32. [Experimental methods and data on heavy organics].
- [50]. L. Carbognani, (1992). Molecular structure of asphaltene proposed for 510c residue of Venezuelan crude, INTEVEP S.A. Tech. Report.
- [51]. S. Priyanto, G.A. Mansoori and A. Suwono, (1998) "Asphaltene micellization and its measurement", Proceedings of the 3rd. International symposium on advanced and aerospace science and technology in Indonesia (ISASTI, 98), Jakarta August 31-September 3, 1998, Vol. 2, ISASTI-98-4.8.8, pp.843-860. [Development of a new experimental procedure and results for micellization of asphaltene].
- [52]. S. Priyanto, G.A. Mansoori and A. Suwono, (2001) "Structure & Properties of Micelles and Micelle Coacervates of Asphaltene Macromolecule", *Nanotechnology Proceed. of 2001 AIChE Annual Meet.*.. [Presentation of the use of asphaltene micelles and micelle coacervates for nanotechnology].
- [53]. S. Priyanto, G.A. Mansoori and A. Suwono, (2001) "Measurement of property relationships of nano-structure micelles and coacervates of asphaltene in a pure solvent" *Chem. Eng. Science*, Vol.56, pp.6933-6939. [A first time novel and simple experimental procedure for measurement of the entire phase diagrams of asphaltene micellization and micelles self-assembly].
- [54]. G.A. Mansoori, (2002) Cause and effect of deposition and fouling of heavy organics and other

compounds in fuel and petrochemical processes, *KU Int'l J Sci. & Tech., Transaction B*, 1-17. [A detailed molecular-based description]

[55]. Rogacheva, O.V., Rimaev, R.N., Gubaidullin, V.Z., and Khakimov, D.K., (1980) "Investigation of the Surface Activity of The Asphaltenes of Petroleum Residues," Ufa Petroleum Institute. Translated from *Kolloidnyi Zhurnal*, Vol. 42, No.3, PP.586-589, May-June 1980. [An excellent pioneering research on this subject].

[56]. Kawanaka, S., Park, S.J. and Mansoori, G.A. (1991) "Organic Deposition from Reservoir Fluids" *SPE Reservoir Engineering Journal*, pp. 185-192, May 1991. [This is the molecular theory behind predicting the onset of precipitation of heavy organics from petroleum fluids].

[57]. S.T. Kim, M.E. Boudh-Hir and G.A. Mansoori, (1990) The role of asphaltene in wettability reversal. In: *Proceedings of the 1990 Annual Convention of the Society of Petroleum Engineers, Richardson, TX* (1990), pp. 120–137 SPE Paper #20700. [Molecular theory of wettability reversal of surfaces due to asphaltene attachment to surface is introduced here along with experimental data].

[58]. C. Lhioereau, J. Briant and R. Tindy, (1967) Influence de la Pression sur la Flocculation des Asphaltenes. *Rev. Inst. Fr. Pet.* **22** , pp. 797–808. [Effect of pressure on asphaltene deposition is presented here].

[59]. Lichaa, P.M., Herrera, L., 1975. Electrical and other effects related to the formation and prevention of asphaltenes deposition. *Soc. Pet. Eng. J.*, paper #5304.

[60]. Park, S.J. and Mansoori, G.A., (1988). Aggregation and Deposition of Heavy Organics in Petroleum Crudes. *International Journal of Energy Sources*, 10: 109-125. [A comprehensive theory of precipitation, steric colloid formation, flocculation and deposition of asphaltene from petroleum fluids],

[61]. S. Acevedo, M.A. Ranaud, G. Escobar, L. Gutierrez and P. Ortega, (1995) Adsorption of asphaltenes and resins on organic and inorganic substrates and their correlation with precipitation problems in production well tubing. *Fuel* **74** , pp. 595–598.

[62]. S.J. Abedi, S. Seyfaie and J.M. Shaw, (1998) Unusual retrograde condensation and asphaltene precipitation in a model heavy oil system. *J. Pet. Sci. Technol.* **16** 3 and 4 , pp. 209–226. [This contains a clever experimental procedure to demonstrate the irreversibility of asphaltene deposition from petroleum fluids].

[63]. J. Escobedo, G.A. Mansoori, C. Balderas-Joers, L.J. Carranza-Becerra and M.A. Mendez-Garcia, (1997) Heavy organic deposition during oil production from a hot deep reservoir: a field experience SPE Paper #38989 . In: *Proceedings of the 5th Latin American and Caribbean Petroleum Engineering Conference and Exhibition, Rio de Janeiro, Brazil, 30 August–3 September (1997)*, p. 9. [The title is self-explanatory]

[64]. S.J. Park, T.Y. Kwak and G.A. Mansoori, (1987) "Statistical Mechanical Description of Supercritical Fluid Extraction and Retrograde Condensation.", *International J. Thermophysics*, **8**, pp. 449-471. [The title is self-explanatory]

[65]. V.A.M. Branco, G.A. Mansoori, L.C. De Almeida Xavier, S.J. Park and H. Manafi, (2001) Asphaltene flocculation and collapse from petroleum fluids, *J. Petrol. Sci. & Eng.*, **32**, 217-230. [A comprehensive molecular model for vle and solid deposition prediction using minimum characterization data].

[66]. S.J. Park and G.A. Mansoori, (1998) "Organic Deposition from Heavy Petroleum Crudes (A FRACTAL Aggregation Theory Approach)", *Proceedings of the UNITAR/UNDP 4th International Conference on Heavy Crudes and Tar Sands, Edmonton, Alberta, August 1988*. [The first discovery about the FRACTAL nature of asphaltene aggregation, its FRACTAL dimension calculation and prediction of heavy organics depositions].

[67]. F.J. Nellensteyn, (1924) The constitution of asphalt. *J. Inst. Pet. Technol.* **10**, pp. 311–323. [A historical description of the nature and function of asphaltenes].

[68]. G.A. Mansoori, (1997) Modeling of asphaltene and other heavy organics depositions. *J. Pet. Sci. Eng.* **17**, pp. 101–111. [Incorporation of molecular, FRACTAL and statistical mechanical concepts for development of predictive models for asphaltene and other heavy organics deposition from petroleum fluids].

- [69]. J.H.P. Sanchez and G.A. Mansoori, (1998) *In situ* remediation of heavy organic deposits using aromatic solvents, Richardson, TX SPE Paper #38966 . In: Proceedings of the 68th Annual SPE Western Regional Meeting, Bakersfield, CA, 11–15 May (1998), p. 13. [This is a detailed analysis and prescription for field engineers to be applied for *in situ* remediation of heavy organic deposits].
- [70]. G.A. Mansoori, (2002) Physicochemical basis of fouling prediction and prevention in the process industry" *J. of the Chinese Institute of Chemical Engineers*, Vol. 33 No. 1, pp.25-32, January 2002. [This is a fundamental study and analysis of variety of foulings which may occur during fluid flow in various industries].
- [71]. P. Papon, J. Leblond, P.H.E. Meijer, and S.L. Schnur, (2006) *The Physics of Phase Transitions: Concepts and Applications*, Springer; 2nd edition. .
- [72]. S.A. Mousavi-Dehghani, M.R. Riazi, M. Vafaie-Sefti and G.A. Mansoori, (2004) An analysis of methods for determination of onsets of asphaltene phase separations, *J. Petrol. Sci. & Eng.*, 42 (2-4): 145-156. [A thorough review and analysis of existing methods for detecting phase separations].
- [73]. J.M. Kosterlitz and D.J. Thouless,(1973) Ordering, metastability and phase transitions in two-dimensional systems - *J. Phys. C: Solid State Phys*, 6, 1181-1203.
- [74]. A. Eliassi, H. Modarres and G.A. Mansoori, (2005) Study of asphaltene flocculation using particle counting method, Proceed. Filtech 2005 (Int'l Conf. & Exhib. for Filtration & Separation Tech.), Vol. I, 506-511, Weisbaden, Ger., Oct. 11-13, 2005. [A laser-based detection for asphaltene flocculation in flowing petroleum fluids].
- [75]. J. Escobedo and G.A. Mansoori, (1997) Viscometric principles of onsets of colloidal asphaltene flocculation in paraffinic oils and asphaltene micellization in aromatics. *SPE Prod. Facil.*, pp. 116–122 May. [A very accurate method for onsets measurements].
- [76]. G.A. Mansoori, (2005) *Principles of Nanotechnology: Molecular-Based Study of Condensed Matter in Small Systems*, World Sci. Pub. Co., Hackensack, NJ. [This teaches the science and engineering graduate students and practicing scientists the principles needed to perform research and development work in the emerging field of nanotechnology].

Biographical Sketch

G.Ali Mansoori received BSc-*ChE* degree from University of Tehran, MSc-*ChE* degree from University of Minnesota, PhD from the University of Oklahoma and his postdoctoral training at Rice University, the latter in 1970. He is a professor of bioengineering, chemical engineering and physics at the University of Illinois at Chicago. He has been a visiting professor at University of Pisa, ITB, University of Kashan, Sharif University of Technology; and a visiting scientist at the Argonne National Laboratory, National Institute of Standards and Technology and CNR-Pisa. He has been a consultant to ARCO, BJ Services, British Petroleum (BP), C3 Int'l-LLC, Chevron Oil Field Services, DuPont, Exxon, Eng. Research Corp., Federation of American Scientists, Harza Eng. Co., Hitachi, Ltd., Hydrotech, IMP, Institute of Catalysis of Novosibirsk-Russia, Mitsubishi Chemicals, Motorola, MUCIA, NIGC, NIOC, Norsk Hydro, PEMEX, PETROBRAS, PetroStat Laboratories, Science Applications., Shell Int'l B.V., Synthetic/Johnson-Matthey, Technology International., The Aníán Community (Reuters), United Nations (UNDP; TOKTEN Project), UOP-LLC, Vista Research. Dr. Mansoori's academic and professional honors include: Academician of the International Academy of Creative Endeavors (science, arts, social issues); Algorithm scientific international award; diploma of honor from Pi Epsilon Tau National Petroleum Engineering Honor Society; honorary academician of the International Eco Energy Academy; Kapitsa gold medal from the Russian Academy of Natural Sciences; medal of fundamental science from UNESCO; recognition of dedicated service award from the fuels & petrochemicals division of AIChE, science medal from *Vezerat a Farhang va Aamozesh Aali*, honorary member of the IRI National Academy of Sciences, undergraduate instructional award from UIC. His research and educational activities include arterial blockage / fouling in petroleum and natural gas industries, atomic and molecular nanotechnology, molecular based study of condensed matter, disease diagnostic methods and therapeutic agents, nanostructures design (nanoclusters, nanoconjugates, nanoparticles), phase transitions, *ab initio* methods, density functional and molecular dynamics simulations, statistical mechanics, thermodynamics. Prof. Mansoori has published over 350 technical papers including seven books.