ELECTROCHEMICAL ENERGY CONVERSION AND STORAGE -BATTERIES, FUEL CELLS AND ELECTROCHEMICAL CAPACITORS

P. A. Christensen

The School of Chemical Engineering and Advanced Materials, Newcastle University, Newcastle upon Tyne, UK.

Keywords: Fuel cells, batteries, supercapacitors, electrocatalysis, redox batteries, metal/air batteries.

Contents

- 1. Introduction
- 2. Electrochemical capacitors
- 2.1. Capacitance and Capacitors
- 2.2. The Electric Double Layer
- 2.3. The Evolution of Supercapacitors
- 2.4. The Characteristics of Symmetric Supercapacitors
- 3.1. The Characteristics of Batteries
- 3.2. Primary Batteries
- 3.2.1 The Leclanché Cell
- 3.2.2. The Alkaline Cell
- 3.2.3. Primary Lithium Batteries
- 3.3. Secondary Batteries
- 3.3.1. The Lead Acid Battery
- 3.3.2. NiCd and NiMH Batteries
- 3.3.3. Li ion Batteries
- 3.3.4. Sulfur Cathode Batteries
- 3.3.5. Charging of Secondary Batteries
- 3.3.6. Charge vs Discharge of Secondary Batteries
- 3.4. The Discharge Characteristic of Batteries
- 3. Batteries
- 4. Hybrid Supercapacitors
- 5. Fuel cells
- 5.1. The Fuel and Oxidant
- 5.2. The Effect of Temperature and Pressure
- 5.3. Connecting Fuel Cells Together: the Bipolar Plate
- 5.4. The 3-Phase Region
- 5.5. The Polarization Curve
- 5.6. The Efficiency of Fuel Cells
- 5.7. Low Temperature Fuel Cells
- 5.7.1. The Alkaline Fuel Cell (AFC)
- 5.7.2. The Proton Exchange Membrane Fuel Cell (PEMFC)
- 5.7.3. Alkaline Anion Exchange Membrane Fuel Cells AAEMFC's
- 5.8. Medium Temperature Fuel Cells
- 5.8.1. The Phosphoric Acid Fuel Cell (PAFC)

5.8.2. The Molten Carbonate Fuel Cell (MCFC) 5.9. High Temperature Fuel Cells: the Solid Oxide Fuel Cell (SOFC) 5.9.1. The Electrolyte 5.9.2. The Anode 5.9.3. The Cathode 5.9.4. The Interconnects 5.9.5. Internal Reforming in SOFC's 5.9.6. Sealing 5.10. The Direct Methanol Fuel Cell (DMFC) 5.10.1. The Anode 5.10.2. The Polymer Electrolyte Membrane and Cathode 5.10.3. The DMFC Present and Future 6. "Hybrid" batteries/fuel cells 6.1. The Metal/Air Battery 6.2. Redox Batteries/Regenerative Fuel Cells 7. Microbial Fuel Cells (MFC's) 8. Conclusion Acknowledgements Glossary Bibliography **Biographical Sketch**

Summary

This chapter seeks to take the reader from basic chemical concepts to a full appreciation of the underlying principles and applications of energy storage in supercapacitors, batteries and fuel cells, and to an understanding of their relative strengths and weaknesses both technically and in a commercial context. The historical development of each type of storage device and the key advances are summarized.

1. Introduction

The photograph in Figure 1 shows Winshields Crag on Hadrian's Wall in beautiful Northumberland, England, a World Heritage Site. For nearly 2000 years, Hadrian's Wall has brooded over the borderlands between Scotland and England. In that time, kings and queens have come and gone, empires have risen and fallen, but not a single gram of coal or milliliter of oil has been made.

There is no doubt that the world is heading towards a major energy crisis (among other major crises) and this is giving impetus to an increasingly urgent search for more sustainable and environmentally friendly means of converting and storing energy.



Figure 1. Winshields Crag on Hadrian's Wall, County of Northumberland, United Kingdom.

This chapter deals with three electrochemical methods of converting and/or storing energy: electrochemical capacitors (also known as supercapacitors or ultracapacitors), batteries and fuel cells. These share common characteristics: they all require two solid electrodes in contact with a solid, liquid or gel electrolyte, the energy storage or conversion processes take place at the phase boundary between an electrode and the electrolyte, and the movement of ions and electrons attendant on the conversion or storage processes are physically separated in space.

The primary difference between electrochemical capacitors on the one hand and fuel cells and batteries on the other is that energy is stored in the former type of device by charging the capacitor from an external electrical power source, whilst in the latter, energy is released from chemicals and converted to electricity. Thus, in electrochemical capacitors no electron transfer (Faradaic) processes take place across the electrode/electrolyte interface; in contrast, in fuel cells and batteries during discharge, electron transfer takes place at the electrodes, and chemical species are reduced at, *i.e.* accept electrons from, the cathode and are oxidized at, *i.e.*, lose electrons to, the anode, with the electrons traveling around the external circuit from anode to cathode.

2. Electrochemical Capacitors

A capacitor is a device that stores energy *via* the charging of two electronically conducting 'plates' separated by an insulating medium, the dielectric; in the simplest capacitor, the dielectric is air. If two metal plates separated by such a dielectric are connected to a Direct Current (D.C.) power supply, electrons will flow from the positive

(+) pole of the power supply to one plate, rendering the latter negatively charged, and from the other plate to the negative (-) pole of the supply, leaving the plates equally and oppositely charged, see Figure 2. It may be useful when considering hybrid supercapacitors to bear in mind that so long as at least one of the plates of the device has a potential that increases linearly with charge (see Figure 2), the device may be considered a capacitor. Charging will continue until the voltage across the capacitor is equal to that imposed by the external supply, or until the dielectric starts to breakdown.



Figure 2. The variation in the potentials of the individual plates of a 3.54×10^{-12} Farad (F) air capacitor during charging. V is the voltage across the plates.

2.1. Capacitance and Capacitors

The relationship between the capacitance or charge storing capacity C in Farads (F), the separation of the plates d and the dielectric constant of the insulator, ε , is:

$$C = A\varepsilon\varepsilon_0/d\tag{1}$$

A is the area of each of the two plates, ε_0 is a constant called the permittivity of free space, 8.854 x 10⁻¹² F m⁻¹ and ε is the dielectric constant. Thus, a typical air capacitor in an electronics kit has an area of 4 cm²; $\varepsilon = 1$ for air, and so for a plate separation of 1 mm the capacitance is 3.54 x 10⁻¹² F. One Farad is an extremely large capacitance, and

values of μ F, nF or even pF (10⁻⁶ F, 10⁻⁹ F or 10⁻¹² F, respectively) are more usually quoted.

As the capacitor charges, the voltage across its plates, V, is given by Eq. (2):

$$C = q/V$$

where q is the charge placed on the positive plate (that generates an equal and opposite charge on the negative plate) in Coulombs, C. The variation in V with q is shown in Figure 3; the energy stored in the capacitor charged to a voltage V is the area under the plot in Figure 3; from simple geometry (the area of a triangle) the area is:

Area = engergy E stored in Joules (J) = 0.5qV

From Eq. (2):

 $E = 0.5 CV^{2}$

From Eqs. (2) and (4) it can be seen that a 1F capacitor can store 1 C of charge at 1 V, or 0.5 Joule of energy. More generally, 1 Joule is defined:

1 Joule = 1 Amp \times 1 V \times 1 s

(5)

(4)

(2)

A typical 1.5 V AA battery holds 2.8 "Ampere hours" (Ahr); *i.e.* 2.8 A for 1 hour at 1.5V, or 2.8 x 3600 x 1.5 = 15120 Joules. The plates of an air capacitor capable of holding such energy at the same voltage would each have an area of $1.5 \times 10^{12} \text{ m}^2$!



Figure 3. The variation in the voltage across the plates, V, of the air capacitor in Figure 2.

To store more energy or charge, a dielectric having a high(er) ε could be employed, the area of the plates increased, V could be increased and d reduced; the development of electrochemical capacitors has exploited all of these options.

Electrochemical capacitors are often referred to as supercapacitors or ultracapacitors, and there is also a modification known as hybrid capacitors. Supercapacitors are charge storage devices which rely simply upon the charging of the electrical double layer of high surface area carbon electrodes in liquid (usually aqueous) electrolytes. Hybrid supercapacitors are a cross between a capacitor and a battery, and are dealt with in more detail after the section on batteries (Section 3) below.

To understand how an electrochemical capacitor works it may be helpful to go back to basics and describe first how the simple treatment of capacitance given above relates to the double layer at the electrode/electrolyte interface.

2.2. The Electric Double Layer

Figure 4 shows a schematic of the Helmholtz model of the double layer at a positive electrode immersed in aqueous electrolyte; 'electrode' is employed rather than 'plate' in electrochemical capacitors. The term 'electrolyte' is usually taken to refer to the salt which dissolves in the solvent to produce solvated oppositely charged ions; *e.g.* table salt, sodium chloride, dissolves in water to produce solvated (aq = aqueous, s = solid) sodium and chloride cations and anions, respectively:



Figure 4. Schematic representation of the Helmholtz model of the electrode/electrolyte interface. IHP = Inner Helmholtz Plane, OHP = Outer Helmholtz Plane. Dipoles are represented by crossed arrows, some are omitted for clarity.

The ions render the solvent conducting. Note, however, that the term 'electrolyte' is often used for the dissolved salt and solvent together. To avoid confusion, the states (s, aq *etc.*) of the various chemical species taking part in cell reactions will be omitted.

As water molecules have a dipole (represented by a crossed arrow – the cross is the electropositive end, *i.e.*, the hydrogen atoms, and the arrowhead the electronegative oxygen atom) they are attracted to the electrode with their dipoles aligned in the direction of the electric field, electronegative oxygen atoms attracted by the positive charge on the electrode. The centers of the adsorbed water molecules form the Inner Helmholtz Plane (IHP). Cations, with their attendant solvation envelope of electrostatically attracted water molecules, are also attracted to the electrode, and their centers form a sheet of charge at the Outer Helmholtz Plane, (OHP).

In effect, the (electrode/IHP) and (IHP/OHP) interfaces form two capacitors in series, the total capacitance C_H of which is given by:

(7)

 $1/C_{\rm H} = 1/C_{\rm IHP} + 1/C_{\rm OHP}$

If the radius of the water molecule is r_{water} and a is the distance from the electrode surface to the OHP, then combining Eqs. (7) and (1) gives:

$$1/C_{\rm H} = Ar_{\rm water} / \varepsilon \varepsilon_0 + A(a - r_{\rm water}) / \varepsilon \varepsilon_0$$
(8)

where ε is the dielectric constant of water. The radius of a typical cation is 2 x 10⁻¹⁰ m, the radius of water is 1 x 10⁻¹⁰ m and the dielectric constant of water = 80. In considerations of the electrode/electrolyte interface, Double Layer capacitances are often quoted in F m⁻², *i.e.*, as $C_{\rm H} / A$, and feeding the above values ($a = 6 \times 10^{-10}$ m) into (8) gives $C_{\rm H} / A = 1.2$ F m⁻². In practice, double layer capacitances have been found to vary between *ca*. 0.05 – 0.5 F m⁻², and so the theoretical value is somewhat high. This is due to the value of ε chosen; $\varepsilon = 80$ assumes that the water molecules are free to rotate and tumble, and so re-orientate if the direction of the electric field changes. This is not the case for the water adsorbed at the electrode, which is unable to move, and the water between the IHP and OHP which has only very restricted mobility. Calculations suggest $\varepsilon = 6$ for the former and 30 for the latter, which gives $C_{\rm H} = 0.27$ F m⁻², in fairly good agreement with experiment- and still a very large value!

This is the first key reason for the large capacitance of electrochemical capacitors: the very small value of d.

2.3. The Evolution of Supercapacitors

Taking the nomenclature employed in the review by Brodd *et al* supercapacitors have evolved through four generations since the NEC Corporation under license from SOHIO first introduced their SupercapacitorTM in August 1978. The first generation supercapacitors were employed to provide backup power for computer and appliance memories and were symmetric in design, *i.e.*, both electrodes comprised high surface

area porous carbon separated by an aqueous electrolyte. Activated porous carbon can have surface areas typically in the range $700 - 2000 \text{ m}^2 \text{ g}^{-1}$, significantly increasing *A* in Eq. (1) above the geometric area of the electrodes, and hence the capacitance; the specific capacitance can be up to *ca*. 4F g⁻¹. This is the second key effect contributing to the high storage capacity of supercapacitors: the very large surface area of the electrodes.

-

- -
- -

TO ACCESS ALL THE **89 PAGES** OF THIS CHAPTER, Visit: http://www.eolss.net/Eolss-sampleAllChapter.aspx

Bibliography

Acres G. J. K. (2001). Recent Advances in Fuel Cell Technology and its Applications. J. Power Sources, 100, 60 - 66. [Useful, broad review of fuel cell technology from the industrial perspective. Accessible to the non-specialist.].

Aricò A. S., Bruce P., Scrosati B., Tarascon J. M. and Van Schalkwijk W. (2005). Nature Materials, 4, 366. [A review of nanomaterials in fuel cells, supercapacitors and batteries].

Brodd R. J. Bullock K. R., Leising R. A., Middaugh R. L., Miller J. R. and Takeuchi E. (2004). Batteries 1977 to 2002. J. Electrochem. Soc., 151, K1 – K11. [Detailed review covering the development of primary and secondary batteries during the period 1977 to 2002; it also provides a useful summary of supercapacitors.]

Christensen P. A. and Hamnett A. (1994). Techniques and Mechanisms in Electrochemistry, Chapman and Hall, London. [General electrochemistry including double layer capacitance].

Christensen P. A., Jin J.-M., Lin W. F. Hamnett A. (2004). [The Identification of CO Adsorbed at Ru and Pt sites on a Polycrystalline Pt/Ru Electrode and the Observation of their Oxidation and Free Interchange under Open Circuit Conditions. J. Phys. Chem. B, 108, 3391 – 339. CO diffusion on RuPt].

De Bruijn F. (2005). The current status of fuel cell technology for mobile and stationary applications. Green Chemistry, 7, 132 – 150. [Review of low and high temperature fuel cells, including detailed cost estimates/projections, power densities and catalyst loadings etc. and state-of-the-art performance data as of Oct. 2004].

Dicks A. L. (2006). The Role of Carbon in Fuel Cells. J. Power Sources, 156, 128 - 141. Review.

Haile S. M. (2003). Fuel Cell Materials and Components. Acta Materiala, 51, 5981 – 6000. [Detailed review of the role of carbon in all types of fuel cell; extremely technical but useful reference material.].

Hamann C. H., Hamnett A. and Vielstich W. (2007) Electrochemistry. Wiley-VCH, 2nd ed., Weinheim. [General text on electrochemistry with reasonably detailed treatment of fuel cells and batteries].

Hamnett A. and Christensen P. A. (2000). Electrochemical and Photoelectrochemical Energy Conversion, in "The New Chemistry", Ed. N. Hall, Ch. 15, pp 407 – 439, Cambridge University Press. [Introduction to fuel cells and batteries].

Jiang S. P. and Chan S. H. (2004). A Review of Anode Materials Development in Solid Oxide Fuel Cells. J. Mat. Sci., 39, 4405 – 4439. [Extremely informative, but highly technical, review of the development of anodes for the SOFC. Excellent reference material.].

Larmanie J. and Dicks A. (2004). Fuel Cell Systems Explained. 2nd edn. Wiley, Chichester, UK. [Detailed treatment of main fuel cell types, problems, advantages etc. Technical Handbook].

Logan B. E., Hamelers B., Rozendal R., Schröder U., Keller J., Freguia S., Aelterman P., Verstraete W and Rabaey K. (2006). *Microbial Fuel Cells: Methodology and Technology* Env. Sci. Technol., 40, 5181 – 5192. [Critical review of microbial fuel cells, useful references for further reading].

Ormerod R. M. (2003). Solid Oxide Fuel Cells. Chem. Soc. Rev., 32, 17 - 28. [Excellent technical review of Solid Oxide Fuel Cell technology; useful summary of the history of SOFC development and a detailed coverage of all the key issues.].

Pan Y. H. (2006). Advanced air-breathing direct methanol fuel cells for portable applications. J. Power Sources, 161, 282 – 289. [Technical paper].

Plitz I., Dupasquier A., Badway F., Gural J., Pereira N., Gmitter A. and Amatucci G. G. (2006). The Development of Alternative Nonaqueous High Power Chemistries. Appl. Phys. A, 82 (2006) 615 – 626. [State-of-the art in hybrid supercapacitor development].

Ramasamy R. P., Feger C., Strange T. and Popov B. N. (2006). Discharge Characteristics of Silver Vanadium Oxide Cathodes. J. Applied Electrochemistry, 36, 487 – 497. [State-of-the-art on silver vanadium oxide battery cathodes].

Reshetenko T. V., Kim H-T., Lee H., Jang M. And Kweon H-J. (2006). Performance of a direct methanol fuel cell (DMFC) at low temperature and cathode optimization. J. Power Sources, 160, 925 - 932. [Technical paper with up-to-date references].

Singhal S. C. and Kendall K. (2004), High-temperature Solid Oxide Fuel Cells: Fundamentals, Design and Applications, Elsevier Science, New York. [Detailed treatment of solid oxide fuel cells].

Song C. (2002). Fuel Processing for Low-temperature and High-temperature Fuel Cells. Challenges and Opportunities for Sustainable Development in the 21st Century. Catalysis Today, 77, 17 - 49. [Detailed review of fuel processing].

Tomczyk P. (2006). MCFC versus Other Fuel Cells-Characteristics Technologies and Prospects. J. Power Sources, 160, 858 – 862. [Brief comparison].

Various. (2002). Faraday Discussions, 121, 349 – 364. [Various detailed discussions on the rôle of CO diffusion in fuel cell electrocatalysis].

Vielstich W., Lamm A. and Gasteiger H. A. (2003). Handbook of Fuel Cells. Vols. 1 - 4, Wiley, Chichester, UK. [Detailed treatment of all aspects of fuel cell science, engineering, technology and application].

Wasmus S. and Kuver A. (1999). Methanol Oxidation and Direct Methanol Fuel Cells: a Selective Review. J. Electroanal. Chem., 461, 14 - 31. [Excellent review of Direct Methanol Fuel Cell technology, somewhat dated but nevertheless extremely useful background information to the technology and its problems.].

Winter M. and Brodd R. J. (2004). What are Batteries, Fuel Cells and Supercapacitors? Chem. Rev., 104 (2004) 4245 – 4269. [Review of energy storage].

Zhang J. P. (2003). The Limitations of Energy Density of Battery/Double-Layer Capacitor Asymmetric Cells. J. Electrochem. Soc., 150, A484 – A492. [Mathematical derivation of a formula to calculate the energy density of hybrid supercapacitors].

Biographical Sketch

Professor P. A. Christensen was born in South Shields, UK on May 28 1960. He was educated at South Shields Grammar Technical School for Boys; Exeter College, Oxford University (B.A. Hons Natural

Sciences Chemistry 1982) and the Royal Institution, London, (Ph. D. under the supervision of Sir George Porter, Oxygen Evolving Photosystems, 1986).

He worked with Dr. Andrew Hamnett as a PDRA in the Inorganic Chemistry Laboratory, Oxford University from 1985 to 1989, after which he took up a Lectureship in Physical Chemistry in the Chemistry Department of Newcastle University. He was promoted to Senior Lecturer in 1996, Reader in 2001 and was awarded a Personal Chair in Pure and Applied Electrochemistry in 2004. He held the position of sub-Dean in the Faculty of Science from 1999 to 2002 and Dean of Graduate Studies in the Faculty of Science, Agriculture and Engineering from 2002 to 2006. In 2002, he moved to the School of Chemical Engineering and Advanced Materials in the University.

PAC was one of the founding Directors of NewChem Technologies Ltd in 2002 and of Clarizon Ltd in 2005, both of which are spin-out companies from Newcastle University, and the latter also from Hong Kong University. In 2006 he joined Gen-X Energy Ltd, a fuel cell company, as Chief Scientist and non-Executive Director. PAC has published over 120 papers on electrocatalysis, photochemistry and *in-situ* Fourier Transform Infrared Spectroscopy, with particular emphasis on water and wastewater treatment and fuel cell development. He has been researching fuel cell electrocatalysis for over 20 years. He co-authored a postgraduate textbook on electrochemistry, "Techniques and Mechanisms in Electrochemistry", London., Chapman and Hall 1994. He has been a member of the Business Development Team of the Fuel Cell Applications Centre (FCAF) since its inception in 2004. The FCAF is part of the Centre for Process Industries, a regional government Centre of Excellence, based in Wilton on Teeside.

©Encyclopedia of Life Support Systems (EOLSS)